

Practical Implications of Coagulation Control

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Introduction

- Installation experience in Ireland.
- Do they work?
- Before and after cost/risk/benefit analyses.
 - Plant B
 - Plant M
 - Plant D
- What have we learned?
 - Some things that CCS won't fix.
 - Commissioning vs Optimisation.
 - Optimisation SCM vs Optimisation UVA/Turbidity
 - Who does what?
 - Maintenance and re-optimisation.
- Working with the operator
- Conclusions
- Remote Access...who is it for?

Installation Experience in Ireland



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But do they work?

- 26 purchased
- First one went in in 2011
- The first 18 were StreamerSense (Streaming Current only)
- The last 8 are CoagSense (UVA, pH, etc.)
- As far as we can tell 4 are not 'working'
 - 2 due to poor coagulant mixing
 - 2 due to the chemistry (pH above 7.5)
- All 4 (from the 18 StreamerSenses) were purchased without the manufacturers involvement
 - No application worksheet
 - No site visit
 - No discussion
- They do work!

Why Automatic Coagulation Control?

- Optimise water treatment
 - Reduce DBPs (enhanced coagulation- Barrier 6).
 - Improve Pathogen Removal (Barrier 4).
 - Reduce Aluminium carryover (Barrier 10).
- Save money (5 years payback).
 - Reduced coagulant usage.
 - Reduced sludge disposal costs.
 - Reduced operator call out costs.

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Plant B - Plant Information

- 27 m³hr⁻¹
- 2 sources
- Crypto detected
- Regularly pumping treated water to waste
- Very variable NOM in low alkalinity low turbidity water
- High Aluminium residuals
- PAC coagulant
- Supplemented by borehole water
- On/off several times a day
- Installed spring 2016
- Optimised and put in control Autumn 2016



Installation Issues: Plant B Layout (before)





Installation Issues: Plant B Layout (after)

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Flocculant addition

2nd static mixer

Coagulant dose (PACI)

Flow meter



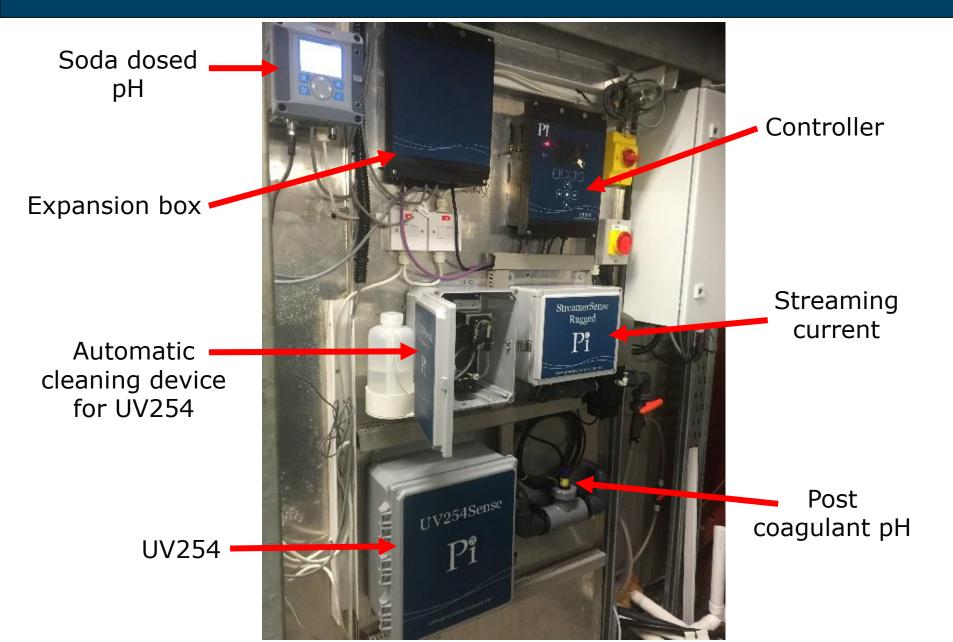
Soda dosed pH sample

1st static mixer (soda dosed just before)

Raw water sump 2 metres outside the wall

Total transit time <45 seconds.

Installation Issues: Plant B Layout



Final Water Turb

Aluminium

Residual

PAC usage

Colour event

Results and Cost Benefit - Plant B

тт	Kesi	lits and Cost Benef	rit – Plant B
		Before Controller Installed	After Controller Installed

0.25 to 0.8 NTU

0.1 to 0.2 mg/l

70-80 PtCo upper limit

80+ PtCo pump to waste

0.05 to 0.1 NTU

0.01 to 0.03 mg/l

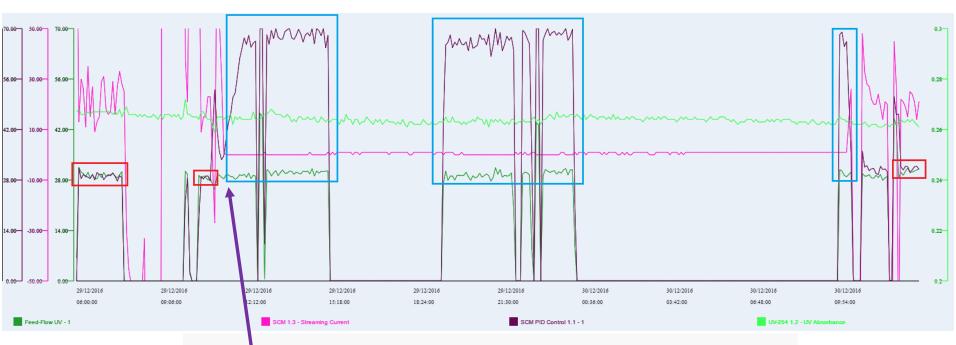
25% reduction

110 PtCo no problem

No longer pumping any

treated water to waste

Validation at Plant B



From Crius - B9BC:A05E:02BF:D5EF < crius@processinstruments.co.uk>

Subject Alarm Active

Alarm message update: 29/12/2016 11:04:53 GMT

Alarm details:

Coagulation Control 1.1

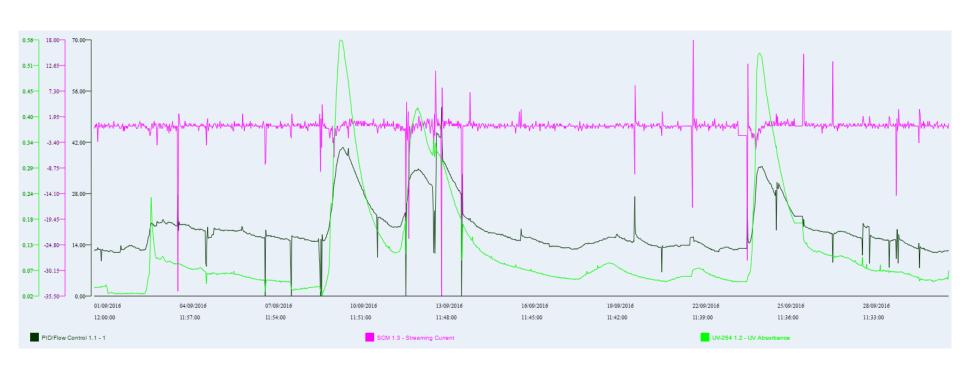
Control input validation error

Control in fail safe

Plant M - Plant Information

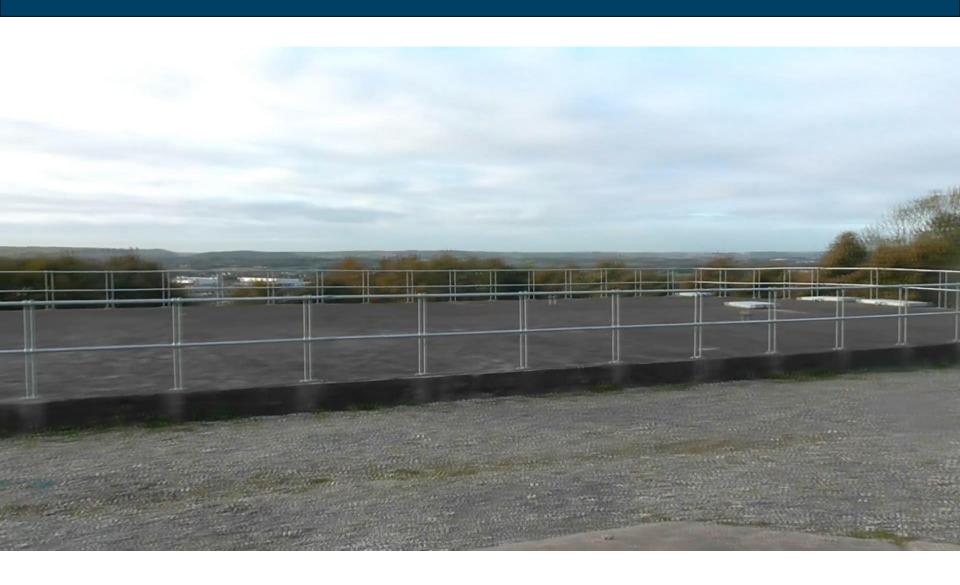
- 128 m³hr⁻¹
- 1 source
- Very variable NOM in low alkalinity low turbidity water
- High Aluminium residuals
- No pH control
- PAC coagulant
- Continuous plant
- Installed spring 2016
- Optimised and put in control Summer 2016

What Does The Data Show Us?



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An Operators View



Residual

Results and Cost Benefit - Plant M

	Before Controller Installed (Jan/Feb 2016)	After Controller Installed (Jan/Feb 2017)	
Settled Water Turb	0.43 NTU	0.34 NTU	

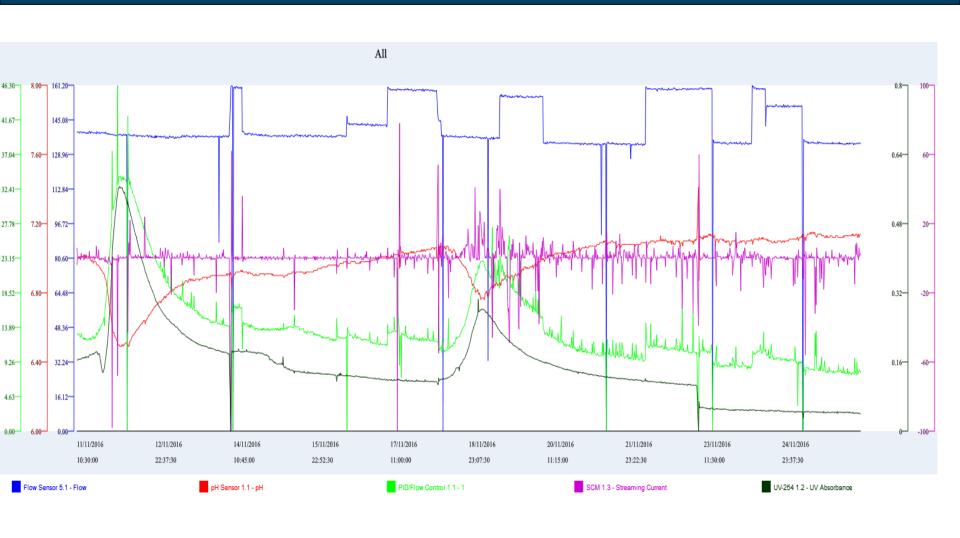
Aluminium 34.01 ug/l 18.40 ug/l Residual

36.58ppm

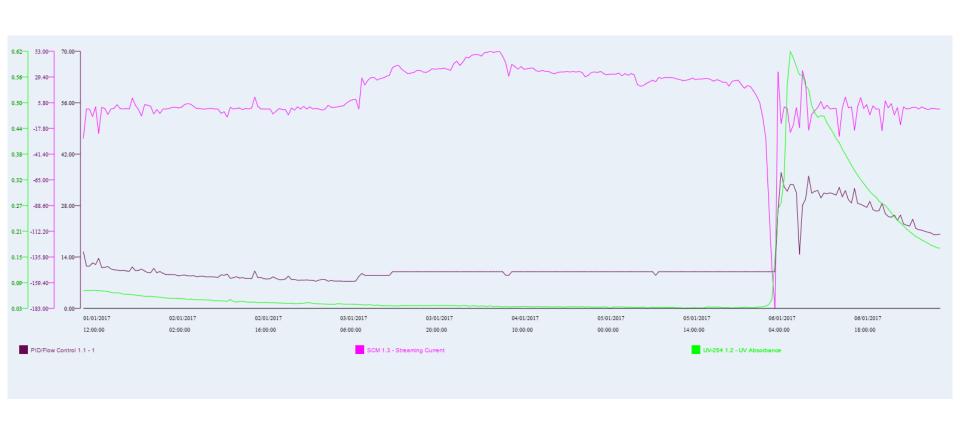
Min 10% reduction 48.94ppm **PAC** usage (€1705) **Aluminium**

Several alum spikes 200ug/l No barrier 10 breaks or

What Does The Data Show Us?



When do they turn it off?



Plant D - Plant Information

- 500 m³hr⁻¹
- 1 source (Influenced by another)
- Very variable NOM in low alkalinity variable turbidity water.
- Soda control.
- Alum coagulant.
- Continuous plant.
- Installed spring 2016.
- Not yet in automatic control.
- Needed control when the operator isn't present.

Results and Cost Benefit - Plant D

Before Controller Installed	After Controller Installed

Final Water

? to NTU ? to NTU **Turbidity**

Aluminium ? to mg/l ? to mg/l Residual

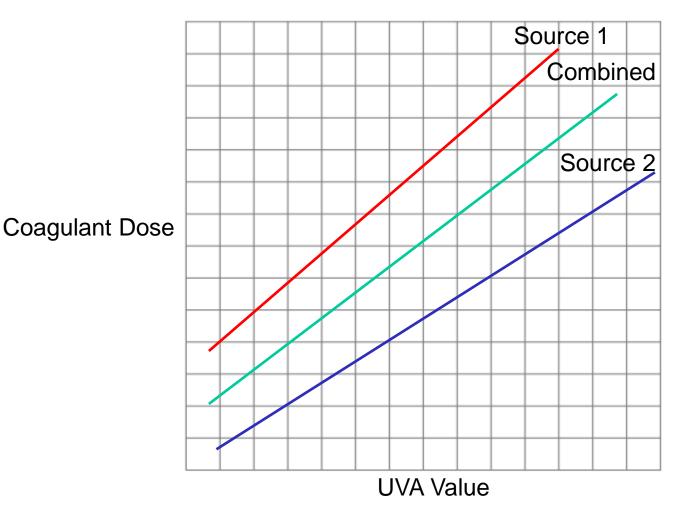
Alum and Soda €14,000 PA (2.5 year payback) **Savings**

- Fundamentals of a Plant
 - Multiple sources and feed forward control.
 - Physical layout.
 - Poor mixing.
 - High energy floc environments.
- Poor Practise
 - Sample point inappropriate.
 - Dosing point inappropriate.
 - Non-dilution of Alum.
 - Dilution of PAC.
 - Poorly sized dosing pump.
 - Poor instrumentation/maintenance (pH)
- If a plant can't run in manual automating it WON'T fix it!
- It also needs looking after! (maintenance)

- Fundamentals of a Plant
 - Physical layout.



- Fundamentals of a Plant
 - Multiple sources and feed forward control.

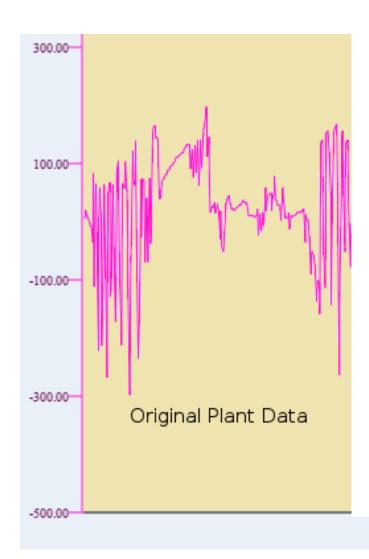


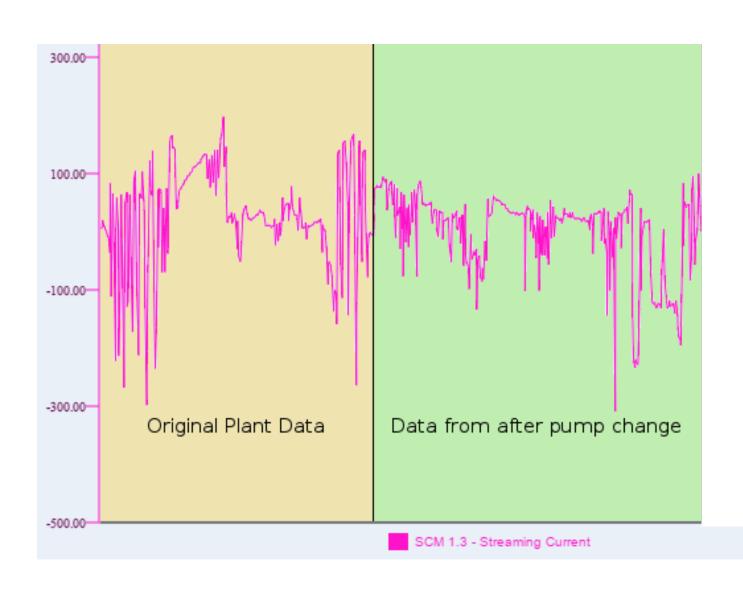


- Fundamentals of a Plant
 - Poor mixing.
 - High energy floc environments.

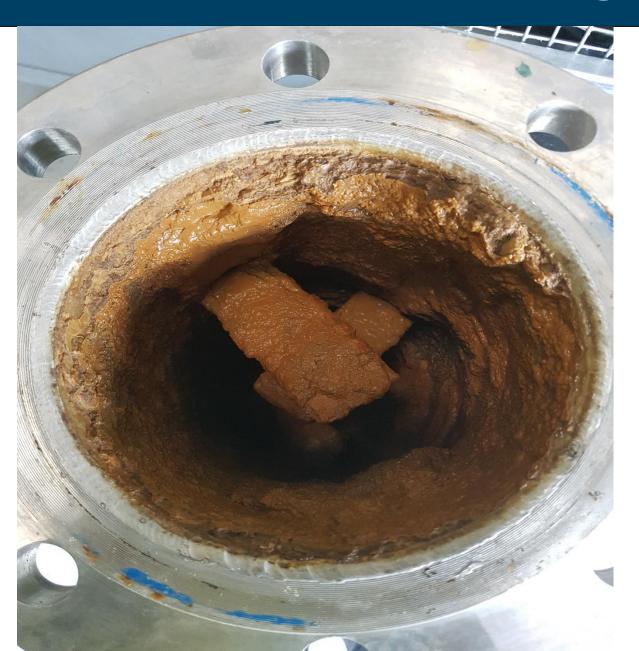


What have we learned?: Pumps and Mixing - Plant R

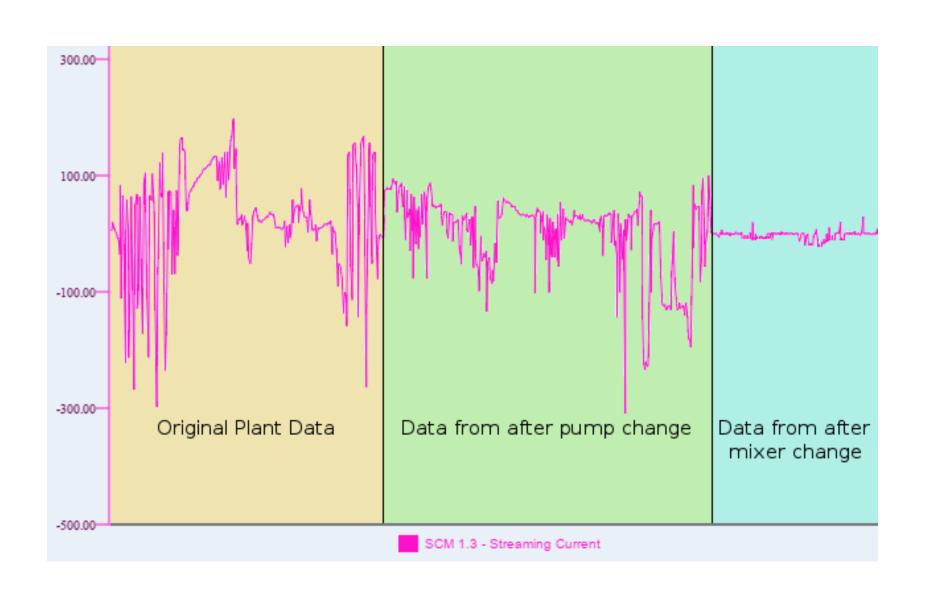




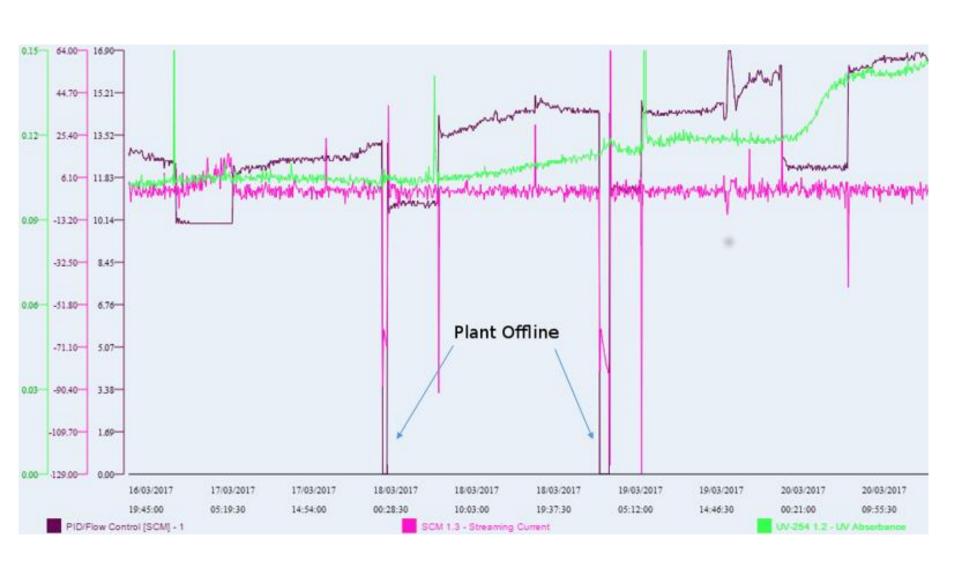








Mixing - Plant R



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What we have learned: Operation and Maintenance

0.00	~	NH4-N	Ammonia -
, 0.00	-	NH4-N	Ammonia -
1.652			Filter 2 Level
-3.499			Final pH
1.584	m		Filter 1 Level
0.461	NTU	TRB	Raw Turbidity
0.036	NTU		Final Turbidity
16.9	°C		Raw Water PH
6.95	pΗ		Raw Water PH

What we have learned - Maintenance



$m P {1}^{"}$ What we have learned - Maintenance



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Control vs Commissioning vs Optimisation

Automatic Control

"The ability to automatically maintain a setpoint in varying conditions".

Commissioning

"Turning a system on and ensuring that all constituent parts are functional".

Optimisation

"Choosing the best setpoint".

Optimising SCM

SCM Value	Plant outcomes	
+100	Slightly high alum residual	
	Good turbidity	
+50	Slightly high alum residual	
	Good turbidity	
+30	Good alum residual	
	Good turbidity	
+10	Good alum residual	
	Good turbidity	
-10	Good alum residual	
	Good turbidity	
-20	Good alum residual	
	Increase in turbidity	
+20	Compromise	

Optimising UVA

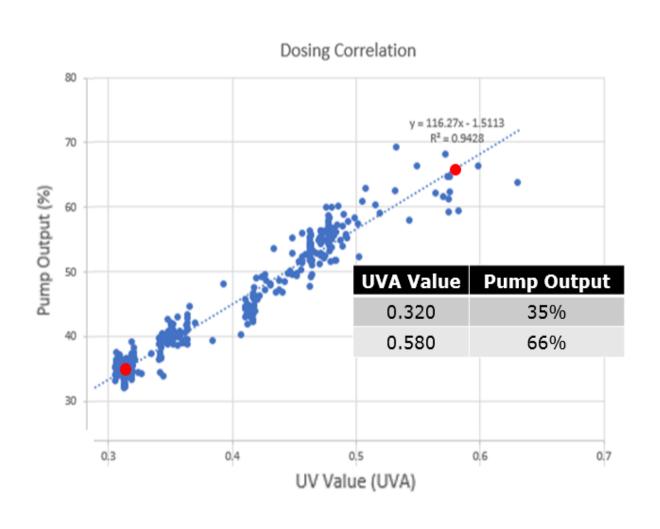
If we have SCM control

If we have don't have SCM

- Plot data dosing data against UVA
- Add more points over time
- Repeated 'tweaking'

- Jar testing
- Multiple times
- Multiple organics levels
- Different seasons
- Repeated 'tweaking'

Optimised UVA Control



$extstyle{ extstyle{1}} extstyle{ extstyle{Who does what - From the beginning}}$

- Get the CCS manufacturer involved.
- Risk/cost benefit analysis.
- Jar testing.
 - Coagulant selection.
 - pH adjustment?
- Get the CCS manufacturer involved.
- Best practice advice on suitability and compliance with IW requirements.
 - Pre-installation checklist.
 - Site visit.
 - Design layout advice.
- Installation Supervision 1 Day
- Commissioning 2 Days
- Optimisation Multiple Days
- Ongoing Operator Support

Pre-Installation Checklist

Technical Note 22 CoagSense Application Questionnaire

Pi are committed to ensuring that you get the best experience from your CoagSense. To ensure that the CoagSense is suitable to meet your coagulation control objectives we need the following information to get every installation right first time, every time. When you have completed the form please email it to your local sales organisation or direct to the factory.

Contact Info				
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-mail				Pi
Nobile No				0 0 0 7 000 01.
lant Name				
own				
Country				
)ate				CRIUS www.pooredisdusements.ast
				0
Application				
. Application type: Water Plan	t, In-plant Process,	DAF, Laundry, Other (e	explain):	
. Batch Process:	_, Occasional Shuto	lowns:, c	or Continuous Online Pr	rocess:
. Quality Water Data (please i	ndicate units):			
Flow Rate	Max:	Min:	Normal:	
TOC (Raw Water)	Max:	Min:	Normal:	
UVA (Raw Water)	Max:	Min:	Normal:	
UVA (Final Water)	Max:	Min:	Normal:	
Turbidity (Raw Water)	Max:	Min:	Normal:	
Turbidity (Settled Water)	Max:	Min:	Normal:	
TDS (Raw Water)	Max:	Min:	Normal:	

Pre-Installation Checklist

	d) lag time from chemical fee	a point to sample t	ake off point:		
Under Max. flow:	seconds, Under M	in. flow:	seconds		
8. Does raw water flow	change widely (+/-30%), and	d/or frequently in a	relatively short time	e (e.g. once per hour).	
Yes No	If Yes, how often or o	quickly:			
9. Is an open, atmosph	eric drain available at sensor	location? Yes	No		
10. Is coagulant curren	tly paced on raw water flow?	Yes No _			
11. Which of the follow	ing instruments are already o	n site and able to p	provide an output for	the CoagSense to use?	
Raw Water	Settled Water	Final Water			
Turbidity:	Turbidity:	Turbidity:			
pH:	pH:	UVA/UVT:			
UVA/UVT:					
If plans include using th	ne CoagSense for Auto-Contro				.2
If plans include using th	ne CoagSense for Auto-Contro chemical on both a raw wate				97
If plans include using the state of the stat		r flow and CoagSer	nse signal, or just the	e CoagSense signal alone	
If plans include using the state of the stat	chemical on both a raw wate	r flow and CoagSer	nse signal, or just the	e CoagSense signal alone	
If plans include using the state of the stat	chemical on both a raw wate	r flow and CoagSer	nse signal, or just the	e CoagSense signal alone	
If plans include using the state of the stat	chemical on both a raw wate	r flow and CoagSer CADA/PLC with a sig	gnal from the CoagSe	e CoagSense signal alone	oagSense?
If plans include using the state of the stat	d control be performed by SC bump accept: 4-20 attach) a line diagram showing etc. Something like this:	r flow and CoagSer CADA/PLC with a signma signal	gnal from the CoagSe	e CoagSense signal alone	oagSense?
2. Will the chemical feed 3. Does chemical feed p Drawing Please draw below (or settling basins, filters, each of the settling basins, each of the sett	d control be performed by SC bump accept: 4-20 attach) a line diagram showing etc. Something like this:	r flow and CoagSer CADA/PLC with a signma signal	gnal from the CoagSo pulse?	e CoagSense signal alone	oagSense?
If plans include using the state of the stat	d control be performed by SC bump accept: 4-20 attach) a line diagram showing etc. Something like this:	r flow and CoagSer CADA/PLC with a signma signal	gnal from the CoagSo pulse?	e CoagSense signal alone	oagSense?

Who does what?

Manufacturer Best Practice

- Pre-installation suitability.
- Equipment spec advice.
- Installation supervision.
- Commissioning.
- Remote data monitoring.
- Correlation implementation.
- UVA/SCM correlation.
- SCM plant optimisation.
- Specialist maintenance.

Customer Best Practice

- Jar testing.
- Coagulant selection.
- Plant mods/Installation
- Pipework mods.
- Equipment installation.
- Routine cleaning.
- UVA/coagulant correlation.
- Offline data recording.
- SCADA Integration.

Working with the Operator

Option 1

- Install, commission, optimise the system.
- Hand the operator a 100 page manual.
- Provide a formal training course delivered with several operators, in front of the boss.
- Require the Operator to sign to say (s)he's been trained

Option 2

- Involve the operator right from the beginning
- Explain 1 to 1 what is trying to be achieved
- Provide personal mobiles to phone for help
- Drop in regularly in the early days
- Provide training 1 to 1
 with no one else around

Introduction

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- Remote Access...who is it for?

Conclusions

- CCSs do work and provide massive benefits not always monetary!
- Be clear on why you are installing coagulation control systems
- Be prepared to find (and fix) stuff you weren't aware of E.g. pumps, mixers, piping etc.
- Involve the manufacturer before, during and after commissioning (ongoing)
- Be clear on the difference between commissioning and optimisation and who does what
- Give the manufacturer and the operator time together
- Encourage the operator to do the routine maintenance and involve the manufacturer with non-routine maintenance.

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Remote Access – Who Is It For?



Thank You

Any Questions?

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Benefits of Automatic Control

- Improve Overall Plant Performance: Consistent, High Quality Finished Water (Barrier 4)
- Optimise Organics Removal (Barrier 6)
- Reduce Chemical Costs (5 year payback)
- Reduce Soluble Aluminum Carryover
- Increase Length of Filter Runs
- Less Sludge Generated
- Less Sludge Disposal Costs
- Operators Able To Focus More On Other Testing and Maintenance
- Fewer Call Outs
- Less Pumping to Waste